

## Group VI Metal Hexacarbonyl Complexes: production, decomposition, modeling

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## Carbonyl collaboration



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## Introduction



#### Motivation

- The hexacarbonyl complex of Sg was synthesized.\*
- It was predicted to be slightly more stable then the complex of its lighter homologue - W(CO)<sub>6</sub>.\*\*
- In our work we aimed at designing an experimental setup for testing this prediction.
- \*J. Even, et al., Science 2014, 345, 1491.
- \*\*C.S. Nash, B.E. Bursten, J. Am. Chem. Soc. 1999, 121, 10830.

## Introduction



#### Stability...

 $\dots$  of transition metal carbonyl complexes can be expressed in terms of M-CO first bond dissociation energies (FBDE)\*.

$M(CO)_6$	Calculated, kJ/mol	Experiment, kJ/mol
$Mo(CO)_6$	171	169
$W(CO)_6$	198	192
$Sg(CO)_6$	205/212	not available

FBDE in turn determines the decomposition behavior of the given complex. Thus by investigating its decomposition, stability of  $Sg(CO)_6$  can be addressed.

\*C.S. Nash, B.E. Bursten, J. Am. Chem. Soc. 1999, 121, 10830.

## Experimental



#### 'Ms.Piggy'...

 $\ldots~^{252} \rm Cf$  spontaneous fission fragment source, located at University of Bern, allows for production:

Rh 107 21.7 m 10.12 700, 100	Rh 108	Rh 109 80 s 17 23, 20, 1 327, 426, 178 291, 113 9	Rh 110	Rh 111 11 s 275,412 231		Rh(CO).
Ru 106 3716 a gr 104 a	Ru 107 3,8 m 0° 3,2 194, 845, 463	Ru 108 4.5 m	Ru 109 34.5 s 17 2 3, 4 2 1926, 226 1929, 359	Ru 110 11.6 b 11.6 b 11.2 vie. 154		Ru(CO) <sub>5</sub>
Tc 105 7.6 m	Tc 106 36 s 276, 2239 1009, 2759	To 107 21.2 s 1 48 1 403, 177 106	Tc 108 5.17 s 7.242 406, 708 733 1554	Tc 109 114 4 150, (29, 96 (9	+ CO/He	Tc(CO) <sub>5</sub>
Mo 104	Mo 105 35.6 s # 49 85.77, 148 361, 250	Mo 106 67.5	Mo 107 3.5 s	Mo 108 1,110 5 2006, 301, 101		Mo(CO) <sub>6</sub>

## Experimental



#### Setup

The following equipment was implemented at 'Ms.Piggy':



Experimental



#### Decomposition column



Decomposition process

 $Mo(CO)_6 \longrightarrow Mo + 6 CO$ 



#### Decomposition curves...

## ...are strongly influenced by **the CO content**, **decomposition surface** and the gas flow rate.





#### Decomposition curves...

## ...are strongly influenced by the CO content, decomposition surface and **the gas flow rate**.



## $Mo(CO)_6$ and $W(CO)_6$

Hexacarbonyl complexes were produced in the following fusion-evaporation reactions at GARIS (RIKEN, Japan) and detected with COMPACT:

<sup>*nat*</sup>Zn(<sup>24</sup>Mg,xn)<sup>87–88</sup>Mo <sup>144</sup>Sm(<sup>24</sup>Mg,xn)<sup>163–164</sup>W

# Significant difference in decomposition behavior was observed:





## Analysis



#### Simulation approach

Implementation of the I.Zvara's Monte-Carlo model of gas adsorption chromatography, coupled to Monte-Carlo simulation of a single-step decomposition reaction, with the following assumptions:

Decomposition...

- …happens only on the surface.
- ...is irreversible.
- ... is a first order kinetics process.
- ...activation enthalpy  $(\Delta H^+) = FBDE$ .

Analysis

$$Mo(CO)_6 \rightleftharpoons Mo(CO)_{6(ads)} \longrightarrow Mo(CO)_{6-x} + xCO$$
  
Simulation



t<sub>ads</sub> is given by I.Zvara's model:

$$t_{ads} = \frac{1}{\nu_{\beta}} \exp{\frac{-\Delta H_{ads}}{RT}}$$

t<sub>r</sub> is calculated from Eyring equation:

$$k = rac{k_b T}{h} \exp rac{\Delta S^+}{R} \exp rac{-\Delta H^+}{RT}$$
 $t_r = rac{1}{k}$ 





By using the least squares fitting of the experimental results with the simulated curves,

 $\Delta S^+$  was found to be 105 J/K/mol.

Results for Mo and W carbonyls



## Prediction



Available theoretical and experimental data were used for simulating the decomposition behavior of Sg carbonyl.

Results for  $Sg(CO)_6$ 



## Prediction



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Results for  $Sg(CO)_6$ 



## Prediction



For a given  $\Delta S^+$  of 105 J/K/mol.





### $Mo(CO)_6$ production yield...

## $\ldots$ is strongly influenced by the ${\bf CO}$ concentration and by the gas flow rate.





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#### Transport time

Retention time of  $Sg(CO)_6$  in a 10 m Teflon capillary is strongly influenced by the temperature and by the gas flow rate.

-∆H <sub>ads</sub> , kJ/mol	T,°C	P, bar	Gas flow, I/min	Retention time, s
54	25	0.7	1.0	70
54	25	0.7	2.0	35
54	25	0.5	2.0	25
54	50	0.5	2.0	5
54	100	0.5	2.0	<1
50	25	0.5	2.0	5
50	15	0.5	2.0	10

#### Detrimental effect of oxygen

Few percent of  $O_2$  in the carrier gas bring the production yield of  $Mo(CO)_6$  to zero. This effect is expected to be even more pronounced with Sg.



Compound	$\Delta H^{\circ}$ , kJ/mol	
MoO <sub>2</sub>	-589	
MoO <sub>3</sub>	-745	
WO <sub>2</sub>	-590	
WO <sub>3</sub>	-843	
*SgO <sub>3</sub>	-874, -951	

\*B. Eichler, A. Türler, and H. Gäggeler, J. Phys. Chem. A, vol. 103, pp. 9296–9306, 1999.





#### CO<sub>2</sub> Oxydation of CO to CO<sub>2</sub> in the *decomposition column* is inevitable if oxygen is present in the carrier gas.



## Conclusions



- We suggested a fast and efficient approach for testing the stability of the group VI carbonyl complexes.
- Experimental results were successfully reproduced by the model both for Mo(CO)<sub>6</sub> and W(CO)<sub>6</sub>.
- Suggested simulation can be used for designing and evaluating data of the future decomposition experiments with Sg(CO)<sub>6</sub>.
- In order to maximize the yield of the Sg carbonyl complex CO concentration and the carrier gas flow rate must be kept as high as possible.
- Oxygen must be constantly monitored and removed from the system efficiently.
- The transport efficiency could be improved drastically by heating up a capillary between RTC and detection unit.

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